

Process optimization and reduction of production costs in modern beet sugar manufacturing

MASTER PLAN

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PRESENTATION OVERVIEW

1. Tailored solution for process development, depending on the technology of treated factory - introduction
2. Master-plan therefore, based on deep process understanding and complex balances of the technology
3. Optimization examples, sorted according to investment and complexity
4. Conclusions, closing remarks

MOTTO

- ✓ how to **reduce the production costs/fossil energy** requirement of the processing
 - ✓ concurrently to **identify the right technologies** to enable the significant **improvement** tailored to the customer needs
 - ✓ all in a **financially viable** manner

Fossil fuel consumption in EU

Stand 1980

1.500 kWh/t_{WS}
4.64MM BTU/ st_{WS}

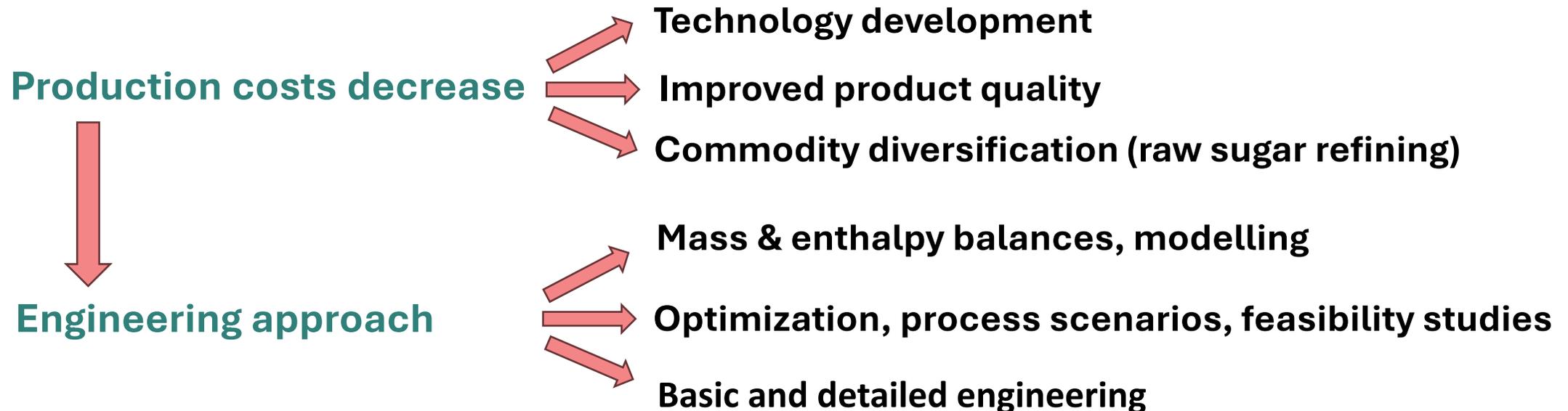
Stand 2020

1.000 kWh/t_{WS}
3.1MM BTU/ st_{WS}

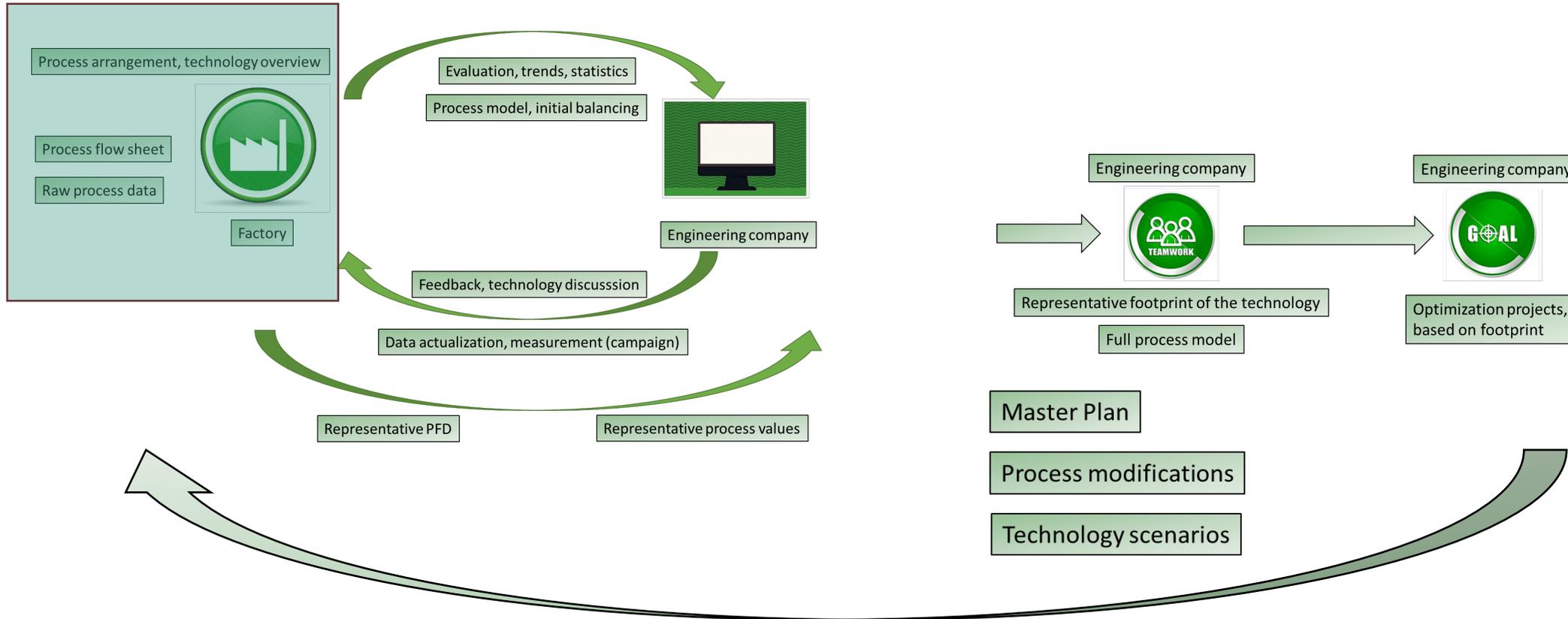
INTRODUCTION - MASTER-PLAN

Reduction of production costs → development projects

Technology analysis → process data → process model → optimization



INTRODUCTION - MASTER-PLAN



INDUSTRIAL EXAMPLES IN OVERVIEW

Master plan: low investment projects, moderate issues and strategical investment

- **Low investment:** Thick juice pre-heating (E1); heating line by pre-limed juice (E2)
- **Moderate investment:** New evaporator bodies (E3); raw sugar refining in beet factories (E4)
- **Strategic investment:** Bio power station (E5); low temperature drying (E6)



E1



E2



E3



E4



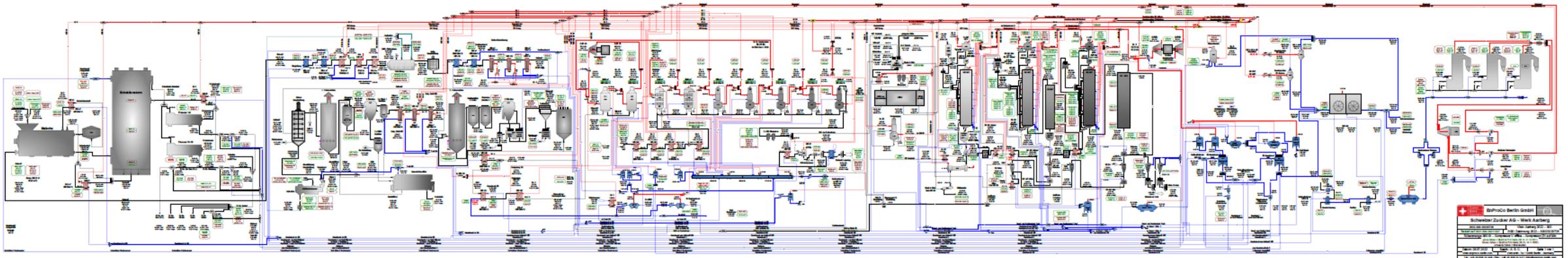
E5



E6

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- Collection and analysis of process data → evaluation and compilation of process model
- Compilation of process model, tailored to the factory processing
- Footprints of the technology, each campaign 2-3 actualizations (good beets, end of campaign, average processing)
- Precision of the model
- **Identification of bottle necks and technology troubles → definition of master plan**



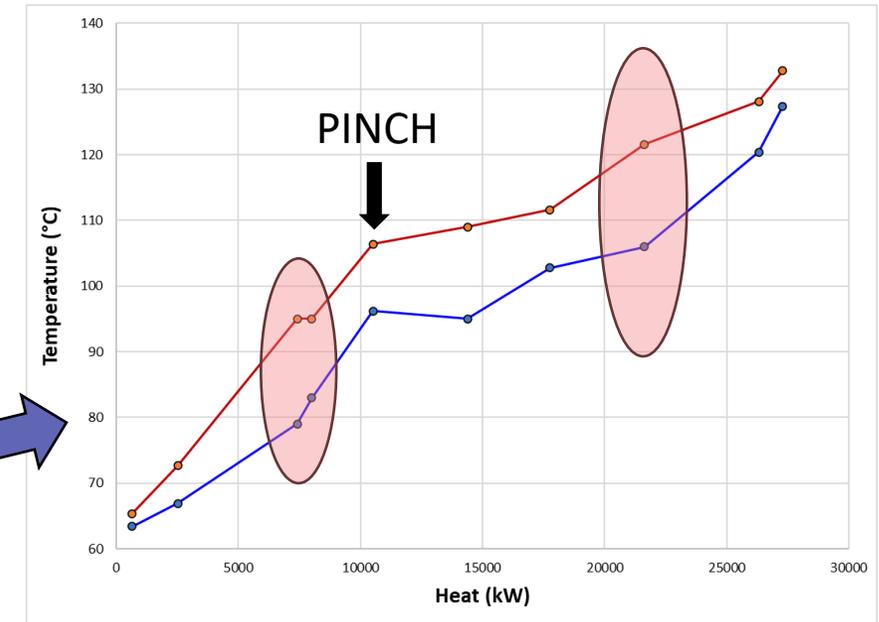
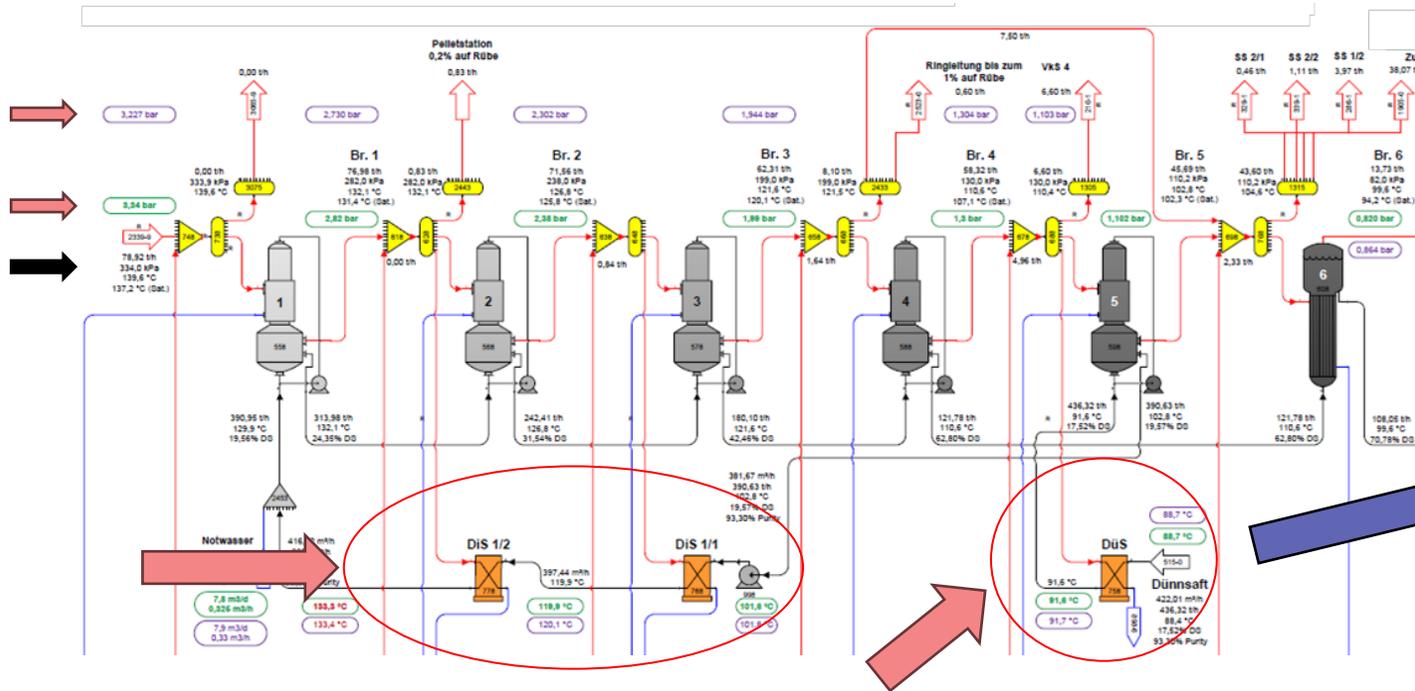
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- Evaluation of process data
- Identification of bottle necks and technology troubles → pinch analysis

Fossil energy consumption

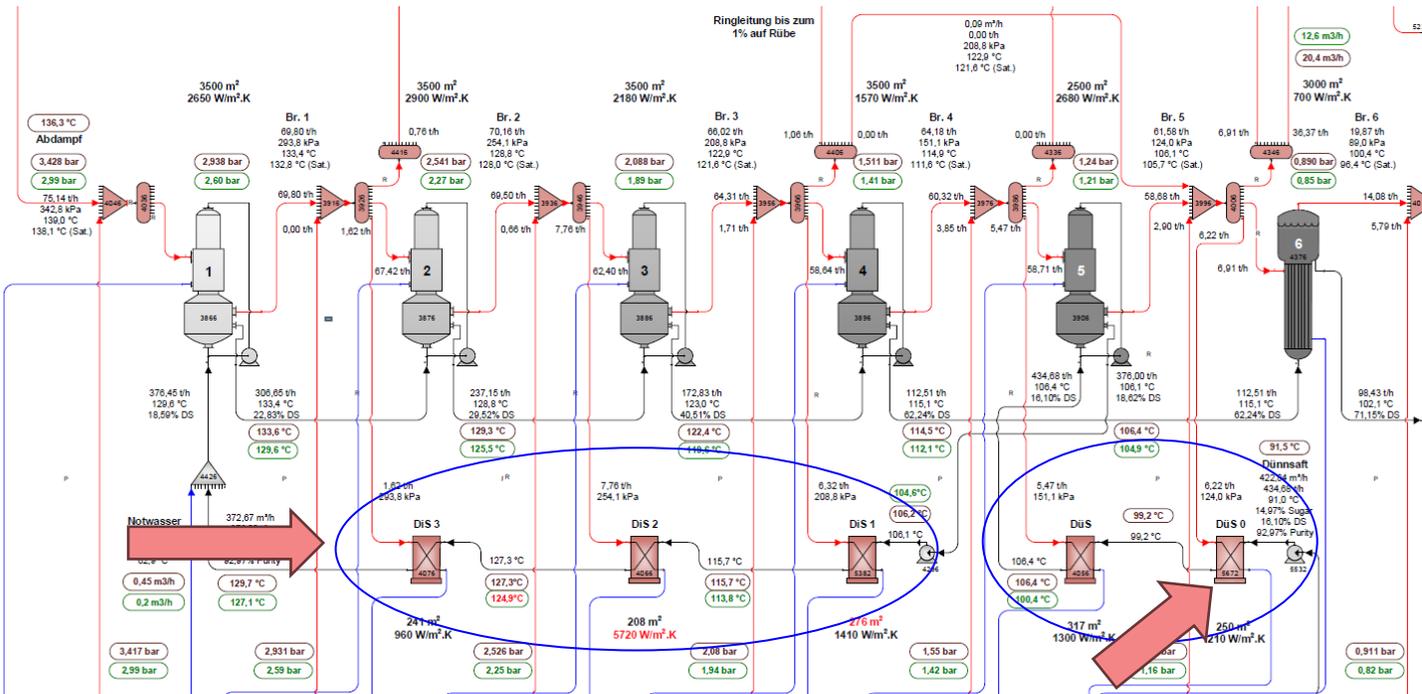
State 2019 1.100 kWh/t_{WS}

3.4MM BTU/ st_{WS}



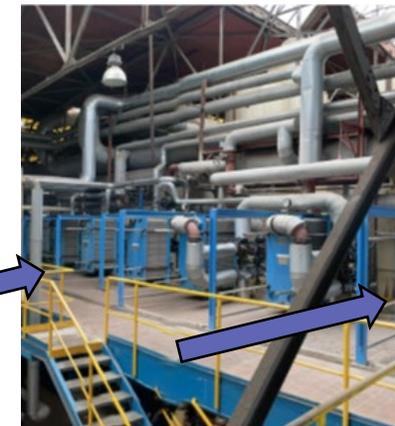
INDUSTRIAL EXAMPLE #1 – LOW INVESTMENT

- **Thick juice pre – heating**
- **Engineering approach: pinch analysis → identification of pinch → modification of heat exchanger → 2 new heat exchangers for Vap5/Vap3 application – minimization of dT before pre-evaporator: higher surface area and better utilization of vapours**



Fossil energy consumption

State 2019 1.070 kWh/t_{WS}
3.31MM BTU/ st_{WS}

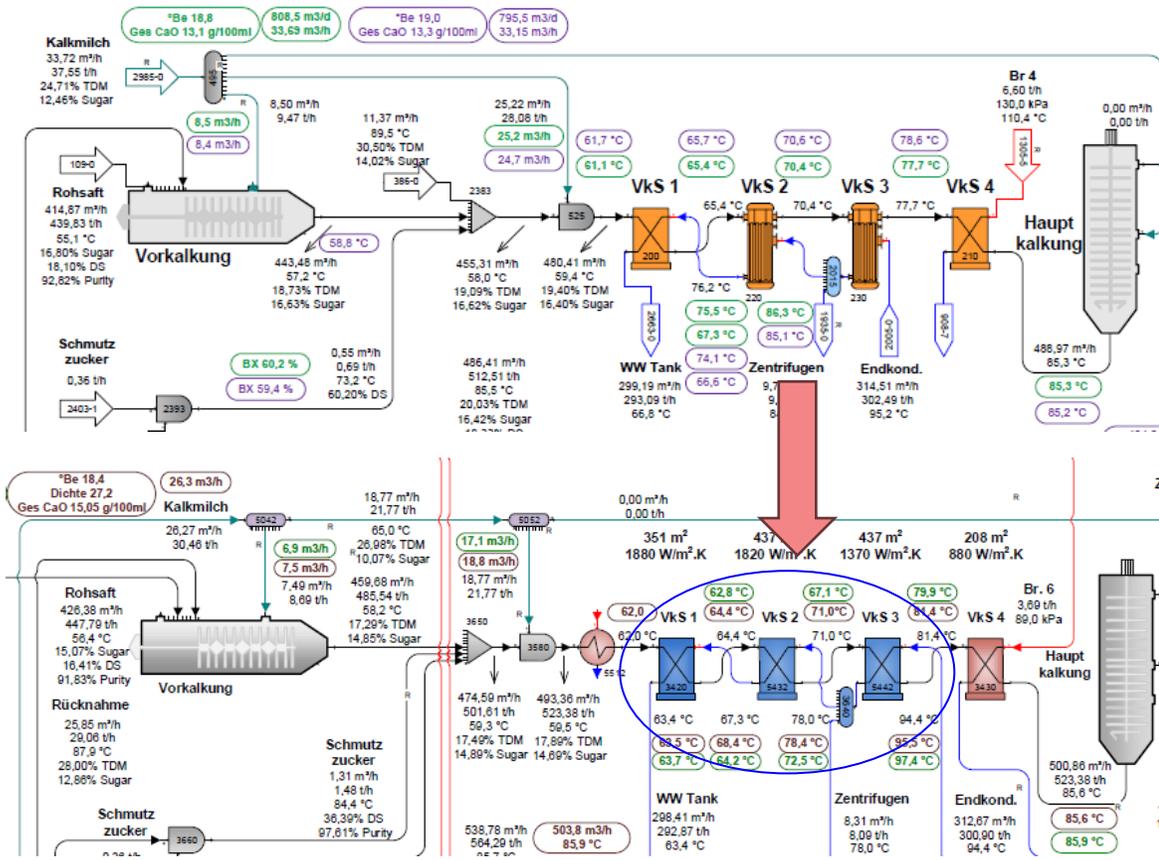




Process Simulation and Consulting in
sugar and chemical technologies

INDUSTRIAL EXAMPLE #2 – LOW INVESTMENT

- **Limed juice – heating**
- **Driving force dT → construction VS heating efficiency → application of plate HEs, k-values**



before

after

Fossil energy consumption

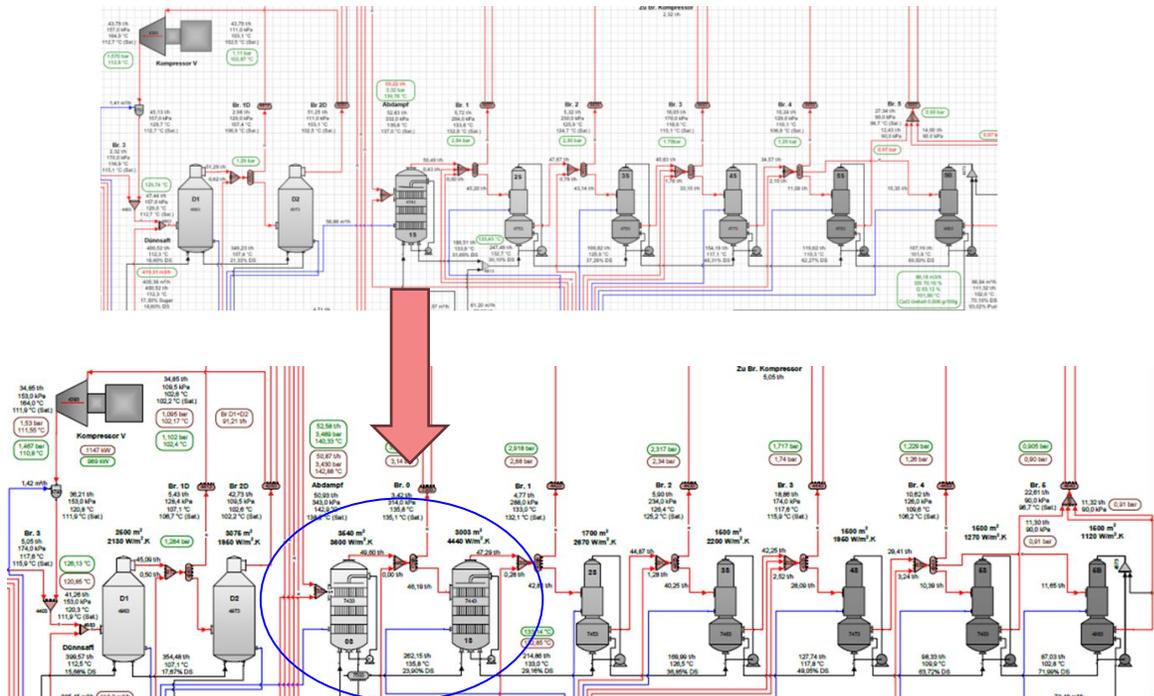
State 2019 1.040 kWh/t_{WS}
3.21MM BTU/ st_{WS}



INDUSTRIAL EXAMPLE #3 – MODERATE INVESTMENT

- **Evaporation station: 6 static effects plus 2 dynamic effects under vapour compression**
- **Extension of static evaporation line: 6 → 7 effects**
- **Based on evaporators analysis → better Δp , better utilization of vapours**
- **Reduction of electrical power for the dynamic evaporation effects**

Fossil energy consumption
State 2024 890 kWh/t_{WS}
2.76MM BTU/ st_{WS}



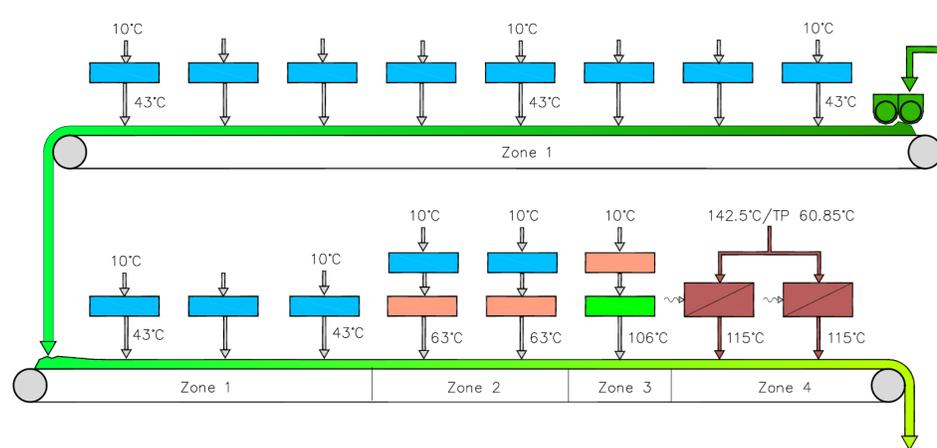
before

after



INDUSTRIAL EXAMPLE #4 – LOW TEMPERATURE DRYING – HIGH INVESTMENT

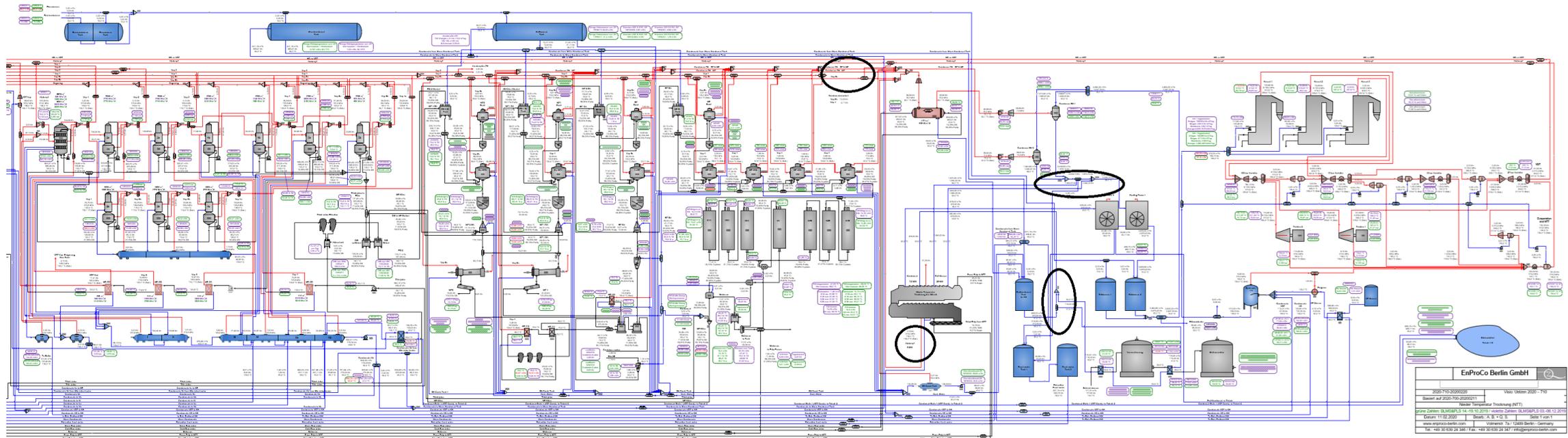
- Excellent example of “green” drying in beet processing, with high investment costs
- Pressed pulp dried with residual heat (**hot water**, **end condensate**, **carbonation vapours**, **boiler house gas-off**)
- Combination of mechanical and thermal water removal from thin pulp layer



Hot condensate	14.5 MW		FW+HC 1'200'000 kg/h Vorlauf 48°C / Rücklauf 37.4°C
Carbo-Vap	3.6 MW		Glykol Carbovrüden 140'000 kg/h Vorlauf 68°C / Rücklauf 45°C
Boiler gas-off			Rauchgas 77'000 kg/h 142.5°C
Hot water	1.25 MW		Heisswasser 68'000 kg/h Vorlauf 120°C / Rücklauf 104°C

INDUSTRIAL EXAMPLE #4 – LOW TEMPERATURE DRYING

- Selection of heat sources in treated factory → balancing, pinch analysis, exergy balance of residual streams
- In detail knowledge of processing technology → essential issue
- Fossil fuel consumption **VERSUS** processing costs VS residual heat balance

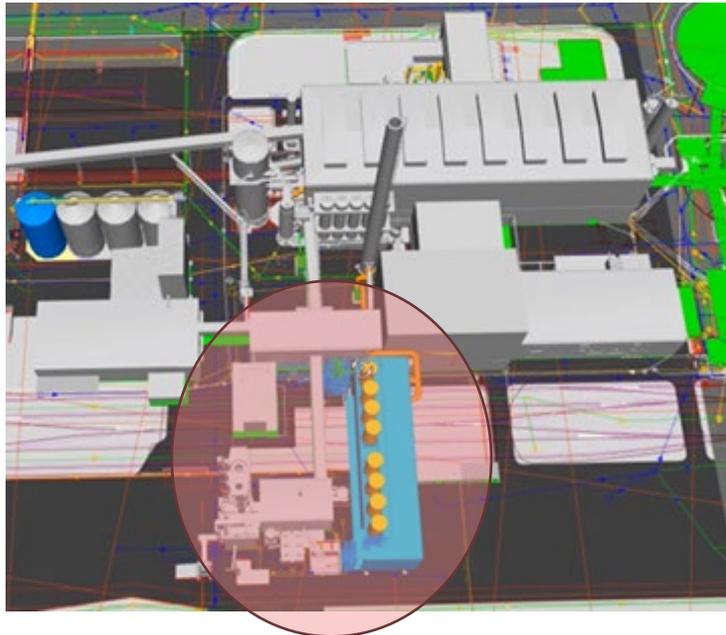


INDUSTRIAL EXAMPLE #4

- Finalisation works in progress, commissioning Summer 2025
- End drying to DS > 96 %
- Project predicted with economy indicators – strong influence of CO₂-emissions

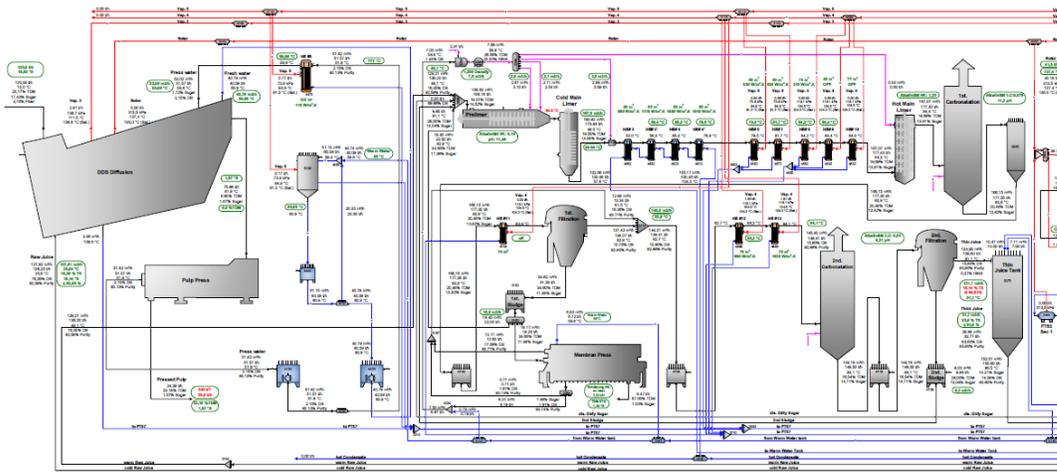
Fossil energy consumption

Prediction 700 kWh/t_{WS}
2.17MM BTU/ st_{WS}



INDUSTRIAL EXAMPLE #5 – RAW SUGAR REFINING - MODERATE INVESTMENT

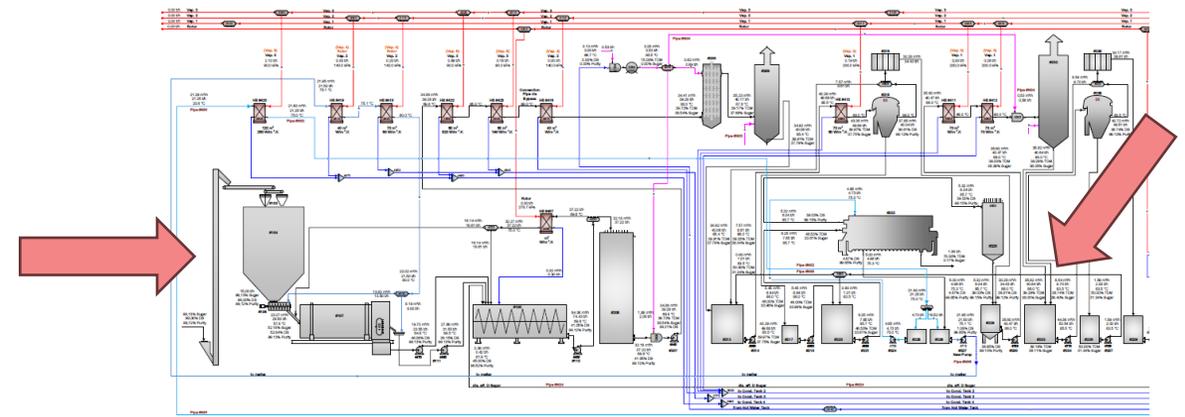
- Raw sugar refining in beet factory? → summer campaign – **mostly sugar house operations**
- Investment for melting and pre-treatment required
- Lime kiln out of performance → CaO external + boiler house gases/booster CO₂
- In the case of good quality of raw sugar → any de-colorization required



Beet campaign

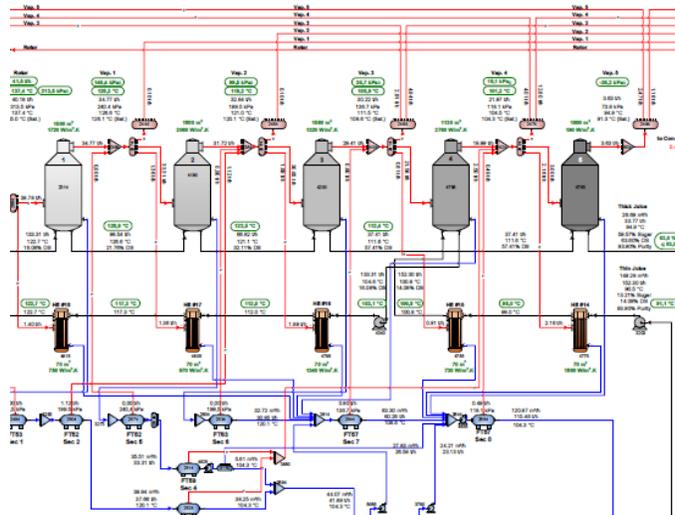
Extraction/melting/purification

Refining campaign



INDUSTRIAL EXAMPLE #5

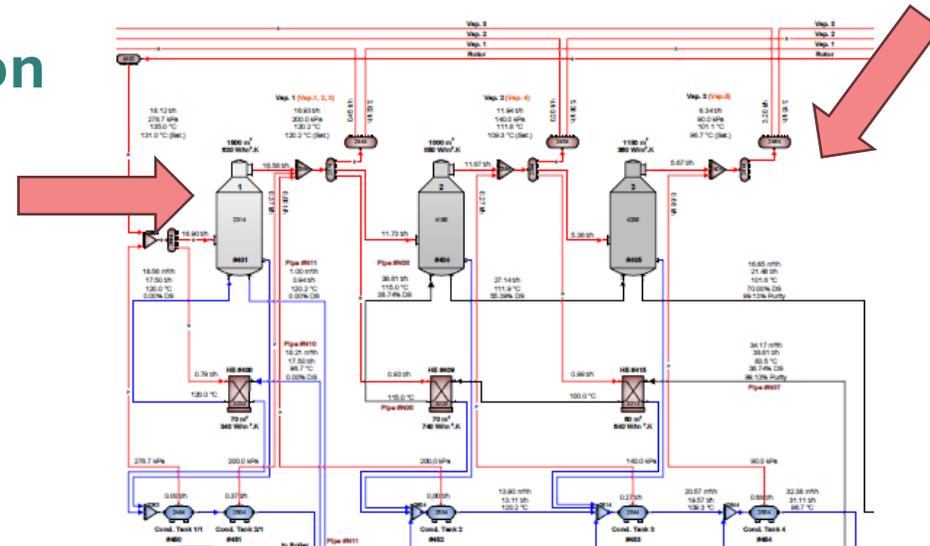
- Raw sugar refining in beet factory → summer campaign
- Evaporation → mostly with moderate budget possible to re-equipped



Beet campaign

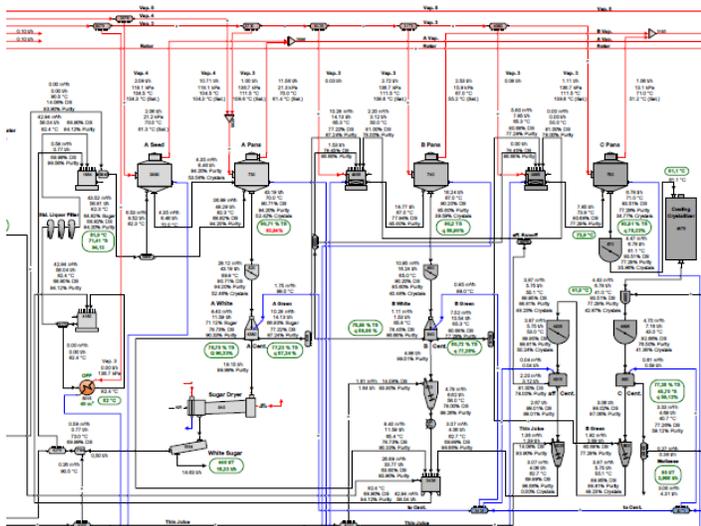
Evaporation

Refining campaign



INDUSTRIAL EXAMPLE #5

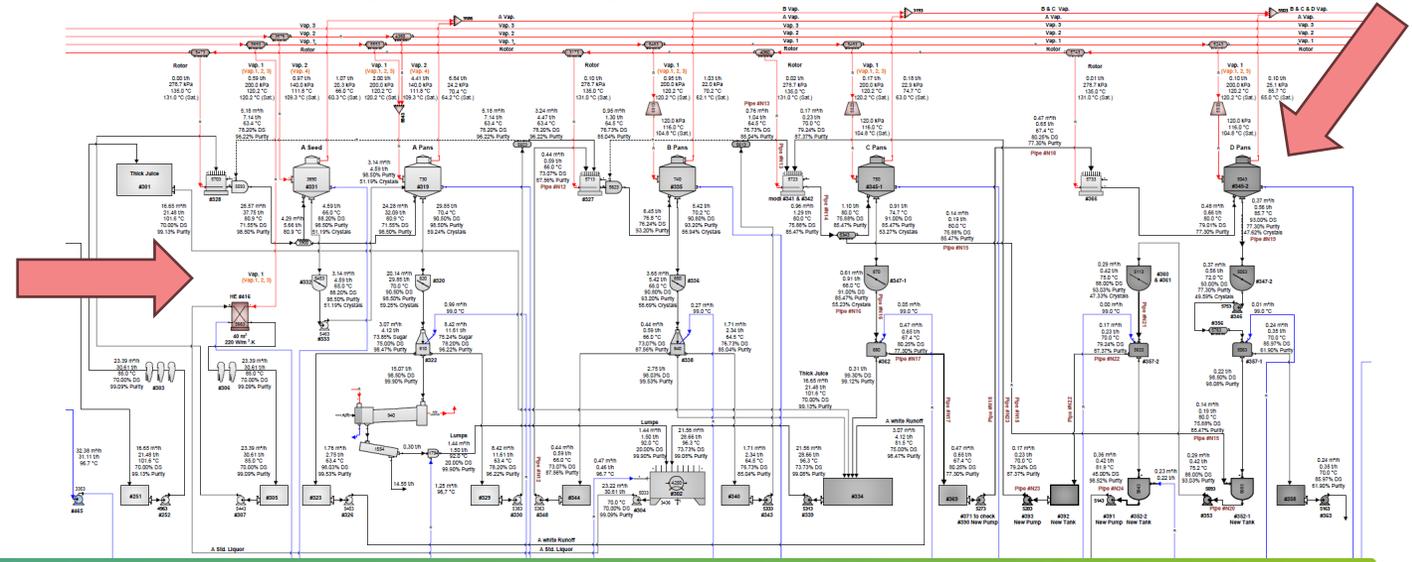
- Raw sugar refining in beet factory → summer campaign
- Success depends on installed machinery → equipment VS sugar loss in molasses



**Beet campaign:
3-product scheme**

Sugar house operations

Refining campaign: 3-strikes + recovery



INDUSTRIAL EXAMPLE #5 – RAW SUGAR REFINING

- **Raw sugar refining in beet factory → summer campaign**
- **Improvement of factory yield → basic & detailed engineering project, realizations 2022, 2024**

Summary:

- **Refining effort depends strongly on installed machinery, especially in sugar house → increase of strikes essential, technology audit required**
- **Melting line, tanks and vessels should be installed, pipework improved**
- **Crucial task is the degradation of sucrose in strikes related to molasses purity → correlation between investment and yield of sugar → feedstock and sugar prices balance**
- **Refining campaign favourable only by reasonable price of feedstock/sugar**

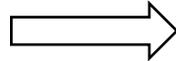
CONCLUSIONS

- **Systematic way to reduce fossil energy with advanced engineering tools**
- **Limitation by conventional technology development (investment)**
- **In EU, the only sustainable solution is the “green” processing**
- **2030 → carbon free production? Renewable energies?**
- **Summer raw sugar refining campaign in beet factory? Possible!**

Official target of EU

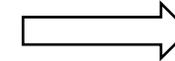
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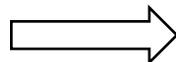
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Fossil energy consumption

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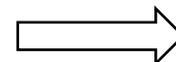


2030

Fossil energy consumption

Prediction 500 kWh/t_{WS}
 1.55MM BTU/ st_{WS}

**Vapour compression, MVR, TVR
Heat pumps**



2035

Fossil energy consumption

Prediction 0 kWh/t_{WS}
 0MM BTU/ st_{WS}

**Carbon free = renewable energies
Bio-boiler house, geothermal energy,
solar/wind**